

# Dynamics of the Auto-Ignition of Biogas in Turbulent Flows

Jhon Alexander Pareja Restrepo



# **Dynamics of the Auto-Ignition of Biogas in Turbulent Flows**

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## **Erklärung**

Hiermit erkläre ich an Eides statt, dass ich die vorliegende Dissertation selbstständig verfasst und keine anderen als die von mir angegebenen Hilfsmittel verwendet habe. Ich erkläre außerdem, dass ich bisher noch keinen Promotionsversuch unternommen habe.

Jhon Alexander Pareja Restrepo

Darmstadt, den 15. April 2019



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A mis padres, Olga y Guillermo



## Abstract

For the development of future energy conversion concepts, sustainable, efficient combustion processes will continue to play a major role. A promising option is the use of renewable sources, such as biomass-derived gasses (biogas). In a variety of present combustion applications, auto-ignition is an essential process. This includes homogeneous charge compression ignition and diesel engines, and burners using flameless combustion. On the other hand, auto-ignition must be prevented in lean premixed pre-vaporized gas turbines or spark-ignition engines. In those practical devices, the fuel and oxidizer flows are highly turbulent. Therefore, understanding the complex, transient and three-dimensional turbulence-chemistry interactions underlying auto-ignition is of high relevance. For that purpose, this work presents an experimental study on auto-ignition of synthetic biogas ( $\text{CH}_4/\text{CO}_2$  mixture). The experimental configuration consists of a fuel jet issuing into a high-turbulence, hot air co-flow to mimic conditions as those of practical devices. The study is focused on two main research aspects, instantaneous two-dimensional (2D) scalar field measurements during the onset of auto-ignition and time-resolved three-dimensional (3D) detection and tracking of auto-ignition kernels. For this purpose, advanced laser-optical diagnostics are adapted for simultaneous multi-parameter measurements.

Instantaneous 2D scalar fields of temperature, mixture fraction and scalar dissipation rate were derived by means of simultaneous Rayleigh scattering and planar laser-induced fluorescence of nitric oxide (NO-PLIF), which enables detecting auto-ignition events, and quantifying the corresponding local mixture fraction and temperature during the onset of auto-ignition. The analysis of these events experimentally confirmed previous fundamental findings from direct numerical simulations (DNS) and experiments which concluded that auto-ignition occurs preferentially in spots (kernels), on isocontours of the so-called most reactive mixture fraction, at locations with low scalar dissipation. A statistical evaluation of the effect of the boundary conditions on the auto-ignition characteristics of biogas showed that, for the presented configuration, neither the Reynolds number of the jet nor the co-flow temperature have a strong influence on the mixture fraction at which auto-ignition occurred. Additionally, it was found that the high level of local anisotropy prevented the onset of auto-ignition.

Regarding 3D transient phenomena, time-resolved tomographic LIF of the hydroxyl radical OH, which combines volumetric laser illumination with a multi-camera detection, was used to study the 3D size, structure, location, and orientation of synthetic biogas auto-ignition kernels and their temporal evolution. Results showed that auto-ignitions occurred in well-defined radial regions of the 3D flow, with strong fluctuations in the main direction of the flow. The statistical evaluation of the orientation and growth of auto-ignition kernels with respect to the mean flow field revealed that the kernels were oriented tangentially to the main flow direction and temporally evolved towards this preferential direction as the ignition event progressed.

Findings derived from the results of the presented work will contribute to better understand the fundamentals of auto-ignition processes and will provide experimental data for validation of numerical simulations and the development and improvement of models.



## Kurzzusammenfassung

In der Entwicklung zukünftiger Energiewandlungskonzepte werden nachhaltige, effiziente Verbrennungsprozesse weiterhin eine wesentliche Rolle spielen. Eine vielversprechende Option liegt in der Verwendung erneuerbarer Energieträger, wie beispielsweise in aus Biomasse hergestelltem Gas (Biogas). In einer Vielzahl heutiger Verbrennungsanwendungen ist Selbstdündung ein unverzichtbarer Prozess. Das schließt homogene Kompressionsdündung und Dieselmotoren ein, sowie Brenner die flammenlose Verbrennung nutzen. Demgegenüber muss Selbstdündung in mager vorgemischten Gasturbinen oder Ottomotoren vermieden werden. In diesen praxisrelevanten Systemen sind die Strömungen von Brennstoff und Oxidator hochgradig turbulent. Daher ist ein Verständnis der komplexen, transienten und dreidimensionalen Turbulenz-Chemie-Interaktionen, die der Selbstdündung zugrunde liegen, von wesentlicher Bedeutung. Zu diesem Zweck wird in dieser Arbeit eine experimentelle Untersuchung der Selbstdündung von synthetischem Biogas ( $\text{CH}_4/\text{CO}_2$  Mischung) vorgestellt. Der Versuchsaufbau besteht aus einem Brennstoffjet, der in einen hohrturbulenten, heißen Coflow aus Luft eingeströmt wird, um die Betriebsbedingungen praxisnaher Apparate nachzubilden. Die Untersuchung legt Gewicht auf zwei wesentliche Aspekte, die zweidimensionale (2D) Messung der Momentanwerte von Skalarfeldern während der Entstehung von Selbstdündung und die zeitaufgelöste, dreidimensionale (3D) Detektion und Verfolgung von Selbstdündungskernen. Dazu werden fortschrittliche Lasermesstechniken für eine simultane Multiparameter erfassung adaptiert.

Momentanwerte der 2D-Skalarfelder von Temperatur, Mischungsbruch und skalarer Dissipationsrate wurden mittels simultaner Rayleigh-Streuung und ebener Laser-induzierter Fluoreszenz an Stickstoffmonoxid (NO-PLIF) abgeleitet. Dies ermöglicht die Detektion von Selbstdündungsereignissen sowie eine Quantifizierung der entsprechenden lokalen Mischungsbrüche und Temperaturen während der Entstehung von Selbstdündung. Eine Auswertung dieser Ereignisse bestätigte experimentell frühere, grundlegende Erkenntnisse aus direkter numerischer Simulation sowie aus Experimenten, die schlussfolgerten, dass Selbstdündung vorzugsweise in Punkten (sog. Kernen) auftritt, an Isolinien des sogenannten reaktivsten Mischungsbruches, an Stellen mit niedriger skalarer Dissipation. Eine statistische Bewertung des Einflusses der Randbedingungen auf die Selbstdündungscharakteristik von Biogas zeigte, dass, für die vorgestellte Konfiguration, weder die Reynoldszahl des Brennstoffjets, noch die Temperatur der Gleichströmung einen großen Einfluss auf den Mischungsbruch haben, an dem Selbstdündung auftritt. Zusätzlich wurde festgestellt, dass ein hoher Grad an lokaler Anisotropie das Eintreten von Selbstdündung verhindert.

Im Hinblick auf transiente 3D-Phänomene wurde eine zeitaufgelöste, tomographische LIF am Hydroxylradikal OH angewendet, die volumetrische Laserbeleuchtung mit einer Mehr-Kamera-Detektion verbindet, um die 3D-Größe, Struktur, Lage und Orientierung von Selbstdündungskernen in synthetischem Biogas zu untersuchen sowie deren zeitliche Entwicklung. Die Ergebnisse zeigen, dass Selbstdündungen in wohldefinierten radialen Regionen der 3D-Strömung auftreten, mit starken Fluktuationen in die Hauptströmungsrichtung. Die statistische Bewertung der Orientierung und des Wachstums der Selbstdündungskerne bezogen auf das mittlere Strömungsfeld zeigte auf, dass die Kerne tangential

zur Hauptströmungsrichtung ausgerichtet sind und sich zeitlich zu dieser Vorzugsrichtung entwickeln während das Selbstzündungseignis fortschreitet.

Die Erkenntnisse, die aus den Ergebnissen der vorgestellten Arbeit abgeleitet sind, werden dazu beitragen die Grundlagen von Selbstzündungsprozessen besser zu verstehen und werden Experimentaldaten zur Validierung numerischer Simulationen bereitstellen sowie für das Entwickeln und Verbessern von Modellen.

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# Nomenclature

## Acronyms

	Description
AI	Auto-Ignition
CCD	Charge-Couple Device
CL	Chemiluminescence
F10	Fuel Blend 90 vol.-% CH <sub>4</sub> /10 vol.-% CO <sub>2</sub>
F20	Fuel Blend 80 vol.-% CH <sub>4</sub> /20 vol.-% CO <sub>2</sub>
F30	Fuel Blend 70 vol.-% CH <sub>4</sub> /30 vol.-% CO <sub>2</sub>
F40	Fuel Blend 60 vol.-% CH <sub>4</sub> /40 vol.-% CO <sub>2</sub>
F50	Fuel Blend 50 vol.-% CH <sub>4</sub> /50 vol.-% CO <sub>2</sub>
FCU	Flow Conditioning Unit
FOV	Field of View
FWHM	Full Width at Half Maximum
IRO	Intensified Relay Optics
JCF	Jet-in-Cross-Flow
JHC	Jet-in-Hot-Coflow
LIF	Laser-Induced fluorescence
LOH	Lift-off-Height
LSF	Line-Spread Function
HT	High Temperature
LT	Low Temperature
MT	Medium Temperature
MTF	Modulation Transfer Function
MWPH	Microwave Plasma Heater
NOx	Nitric Oxides
PIV	Particle Image Velocimetry
PLIF	Planar Laser-Induced Fluorescence

Description	
PSF	Point-Spread Function
SMART	Simultaneous Multiplicative Algebraic Reconstruction Technique
SNR	Signal-to-Noise Ratio
SRF	Step Response Function
SVD	Singular Value Decomposition

## Greek Symbols

	Description	Unit
$\delta$	Outer length scale	mm
$\delta_{0.05}$	Local outer scale full-width where $u$ reaches 5% of $u_c$	mm
$\delta_{1/2}$	Local half-width at half-maximum of velocity profile	mm
$\nabla I_T$	3D gradient of tomographic OH signal intensity	a.u.
$\Gamma$	Normalized spectral overlap fraction	-
$\kappa_\nu$	Spectral absorption coefficient	$\text{cm}^{-1}$
$\Lambda$	Scaling constant for turbulent round jets	-
$\lambda_D$	Strain-limited scalar diffusion scale	$\mu\text{m}$
$\lambda_B$	Batchelor scale	$\mu\text{m}$
$\lambda_{MW}$	Microwave wavelength of the test rig	m
$\xi$	Mixture fraction	-
$\xi_{AI}$	Auto-ignition mixture fraction	-
$\xi_{cl}$	Centerline mixture fraction	-
$\xi_{MR}$	Most reactive mixture fraction	-
$\xi_{NO}$	Mixture fraction from NO-PLIF	-
$\xi_{Ray}$	Mixture fraction from Rayleigh scattering	-
$\xi_{st}$	Stoichiometric mixture fraction	-
$\rho_{coflow}$	Co-flow density	$\text{Kgm}^{-3}$
$\rho_{jet}$	Jet density	$\text{Kgm}^{-3}$
$\sigma_{di}$	Standard deviation of $d_i$	mm
$\sigma_{air}$	Differential Rayleigh scattering cross-section of air	-
$\sigma_{CH4}$	Differential Rayleigh scattering cross-section of methane	-
$\sigma_{CO2}$	Differential Rayleigh scattering cross-section of carbon dioxide	-
$\sigma_{fuel}$	Differential Rayleigh scattering cross-section of the fuel	-
$\sigma_{He}$	Differential Rayleigh scattering cross-section of helium	-

	Description	Unit
$\sigma_i$	Differential Rayleigh scattering cross-section of the species $i$	-
$\sigma_{mix}$	Mixture-averaged differential Rayleigh scattering cross-section	-
$\sigma_{N2}$	Differential Rayleigh scattering cross-section of nitrogen	-
$\sigma_{ox}$	Differential Rayleigh scattering cross-section of the oxidizer	-
$\theta$	Momentum radius	mm
$\nu_{coflow}$	Kinematic viscosity of the co-flow	$\text{m}^2\text{s}^{-1}$
$\nu_{jet}$	Kinematic viscosity of the fuel jet	$\text{m}^2\text{s}^{-1}$
$\chi$	Scalar dissipation rate	$\text{s}^{-1}$
$\chi_{AI}$	Scalar dissipation rate at auto-ignition zone	$\text{s}^{-1}$
$\chi_x$	Scalar dissipation rate axial component	$\text{s}^{-1}$
$\chi_y$	Scalar dissipation rate radial component	$\text{s}^{-1}$

## Latin Symbols

	Description	Unit
$A_j$	Einstein coefficient for spontaneous emission	$\text{s}^{-1}$
$A_{opt}$	Rayleigh scattering collection system efficiency	-
$B_{12}$	Einstein coefficient for stimulated absorption	$\text{m}^3\text{J}^{-1}\text{s}^{-2}$
$\overline{BG}_{HT}$	Background signal at high temperature	a.u.
$\overline{BG}_{Ray}$	Rayleigh background signal	a.u.
$\overline{BG}_{RT}$	Background signal at room temperature	a.u.
$C_{opt}$	NO-PLIF collection system efficiency	-
$D_{coflow}$	Coflow nozzle outer diameter	mm
$D_{coflow,hyd}$	Coflow nozzle hydraulic diameter	mm
$d_i$	Displacement of a kernel pair along the $i$ -direction	mm
$D_{i,coflow}$	Coflow nozzle inner diameter	mm
$\bar{d}_i$	Mean of $d_i$	mm
$D_{j,c}$	Mass diffusivity of jet in the co-flow	$\text{m}^2\text{s}^{-1}$
$d_{jet}$	Jet nozzle diameter	mm
$d_r = (d_y^2 + d_z^2)^2$	Displacement of a kernel pair along the radial direction	mm
$E$	Shot-to-shot laser energy reference	a.u.
$e_r$	Unit vector along radial direction	-
$e_x$	Unit vector along axial direction	-

	Description	Unit
$f_B$	Boltzmann fraction of molecules in the grounds state	-
$I_{bg}$	CL background signal intensity of the “no-flame” region	a.u.
$I_{flame}$	Characteristic CL signal intensity of the flame region	a.u.
$I_\nu^0$	Normalized spectral laser irradiance	$\text{Wcm}^{-2}\text{cm}^{-1}$
$I_{surf}$	OH signal level for AI kernels detection	a.u.
$I_{thresh}$	Adaptive CL signal intensity threshold	a.u.
$I_T$	Tomographic reconstructed OH signal intensity	a.u.
$J_0$	Source momentum flux	N
$k$	Boltzmann constant	$\text{JK}^{-1}$
$K_{i,j}$	$i$ -th kernel detected in the $j$ -th shot	-
$k_r$	Angle between $\mathbf{l}_1$ and $\mathbf{e}_r$	rad
$k_x$	Angle between $\mathbf{l}_1$ and $\mathbf{e}_x$	rad
$\mathbf{l}_1$	Vector along the major axis of a kernel fixed coordinate	-
$l_i$	Feret diameter along the $i$ -direction	mm
$\dot{m}$	Mass flow rate	$\text{Kgs}^{-1}$
$\dot{m}_{axial}$	Axial air injection mass flow rate	$\text{Kgs}^{-1}$
$\dot{m}_{coflow}$	Co-flow mass flow rate	$\text{Kgs}^{-1}$
$\dot{m}_{cool}$	Cooling air mass flow rate	$\text{Kgs}^{-1}$
$\dot{m}_{jet}$	Jet mass flow rate	$\text{Kgs}^{-1}$
$\dot{m}_{seeding}$	Seeding air mass flow rate	$\text{Kgs}^{-1}$
$\dot{m}_{tang}$	Tangential air mass flow rate	$\text{Kgs}^{-1}$
$N$	Number density	$\text{m}^{-3}$
$N_K$	Number of kernels used for any computation	-
$N_{NO}$	Number density of NO	$\text{m}^{-3}$
$P$	Pressure	Pa
$P_{80}$	80th percentile	-
$P_{LOH}$	Accumulative probability of the LOH	-
$p_{thresh}$	CL threshold level	%
$Q$	Electronic quenching rate	$\text{s}^{-1}$
$Re_{coflow}$	Bulk Reynolds number of the co-flow	-
$Re_\delta$	Outer Reynolds number	-
$Re_{jet}$	Bulk Reynolds number of the jet	-
$\overline{S}_{G,air}$	Mean air reference raw signal	a.u.
$S_N$	NO fluorescence signal intensity	a.u.
$S_{N,ox}$	NO fluorescence signal intensity of the oxidizer	a.u.
$S_R$	Rayleigh scattering signal intensity	a.u.
$\overline{S}_{R,air}$	Air reference Rayleigh measurement	a.u.

	Description	Unit
$S_{Ratio}$	Normalized Rayleigh signal	a.u.
$\bar{S}_{R,He}$	Helium reference Rayleigh measurement	a.u.
$T$	Temperature	K
$T_{AI}$	Auto-ignition temperature	K
$T_{coflow}$	Co-flow temperature	K
$T_{control}$	Co-flow control temperature	K
$T_{jet}$	Fuel jet temperature	K
$U$	Absolute streamwise velocity	$\text{ms}^{-1}$
$u$	Excess streamwise velocity	$\text{ms}^{-1}$
$U_{coflow}$	Bulk exit velocity of the co-flow	$\text{ms}^{-1}$
$u_c$	Local outer excess centerline velocity	$\text{ms}^{-1}$
$U_{jet}$	Bulk exit velocity of the jet	$\text{ms}^{-1}$
$W_{fuel}$	Molecular weight of the fuel	$\text{gmol}^{-1}$
$W_{mix}$	Molecular weight of the mixture	$\text{gmol}^{-1}$
$W_{NO}$	Molecular weight of NO	$\text{gmol}^{-1}$
$W_{ox}$	Molecular weight of the oxidizer	$\text{gmol}^{-1}$
$x$	Axial $x$ -coordinate	mm
$X_{fuel}$	Mole fraction of the fuel	-
$X_i$	Mole fraction of the species $i$	-
$y$	$y$ -coordinate	mm
$Y_{fuel}$	Mass fraction of the fuel	-
$Y_{fuel,0}$	Mass fraction of the fuel at the nozzle exit	-
$Y_{NO}$	Mass fraction of NO	-
$Y_{NO,fuel}$	Mass fraction of NO in the fuel	-
$Y_{NO,ox}$	Mass fraction of NO in the oxidizer	-
$z$	$z$ -coordinate	mm

## Dimensionless Numbers

	Description
Re	Reynolds number
Sc	Schmidt number